

Determining Unknown Boundary Conditions in Fluid-Thermal Systems Using
the Dynamic Data Driven Application Systems Methodology

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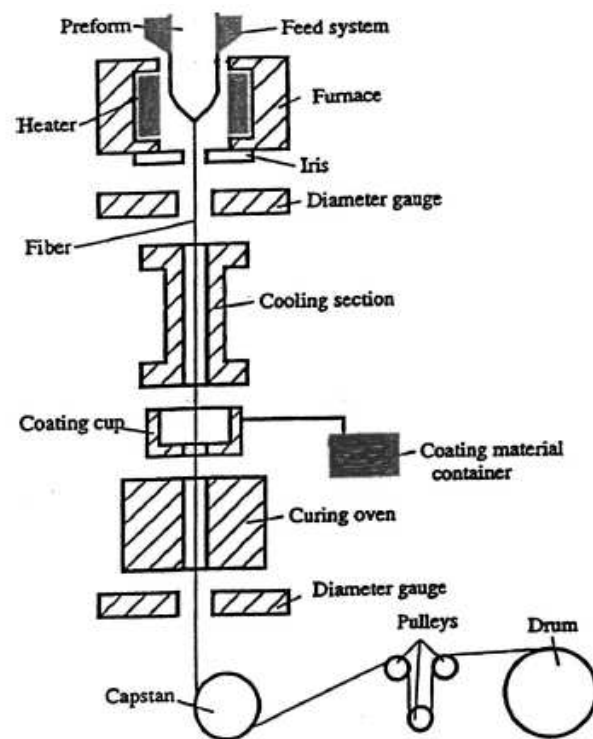
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Outline

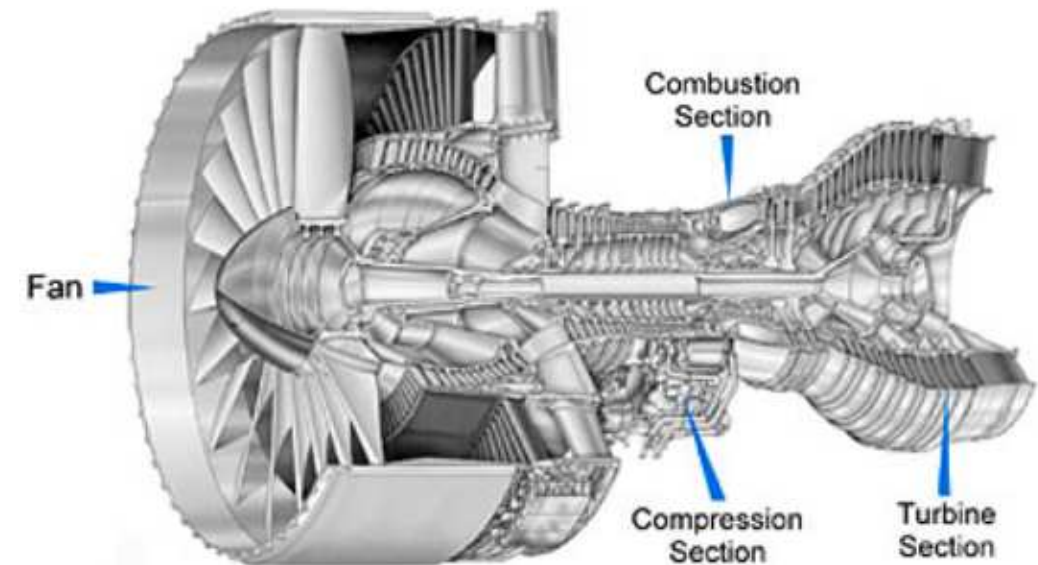
- Introduction
- Problem Definition
- Dynamic Data Driven Applications System Methodology
- Results
- Conclusions

Introduction

- In many engineering applications involving fluid-thermal systems, detailed quantitative information on the flow, temperature and species concentration is needed for system optimization



Optical fibre furnace

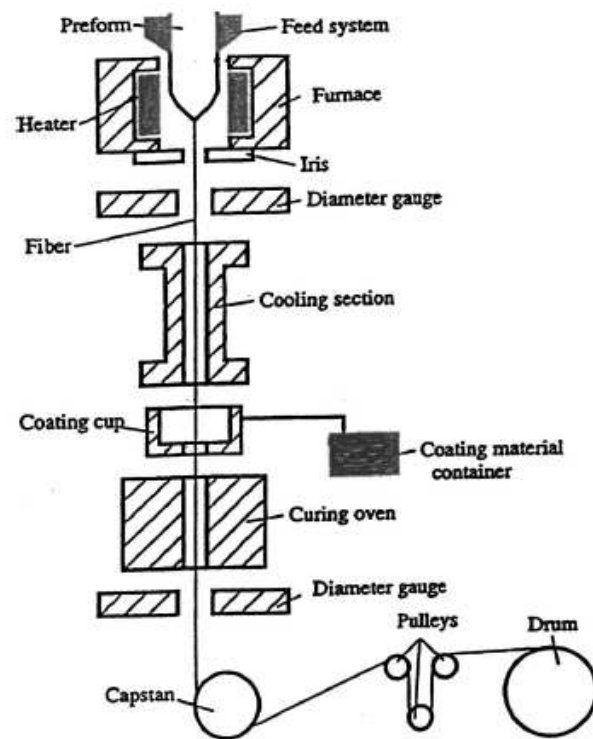


Turbofan engine

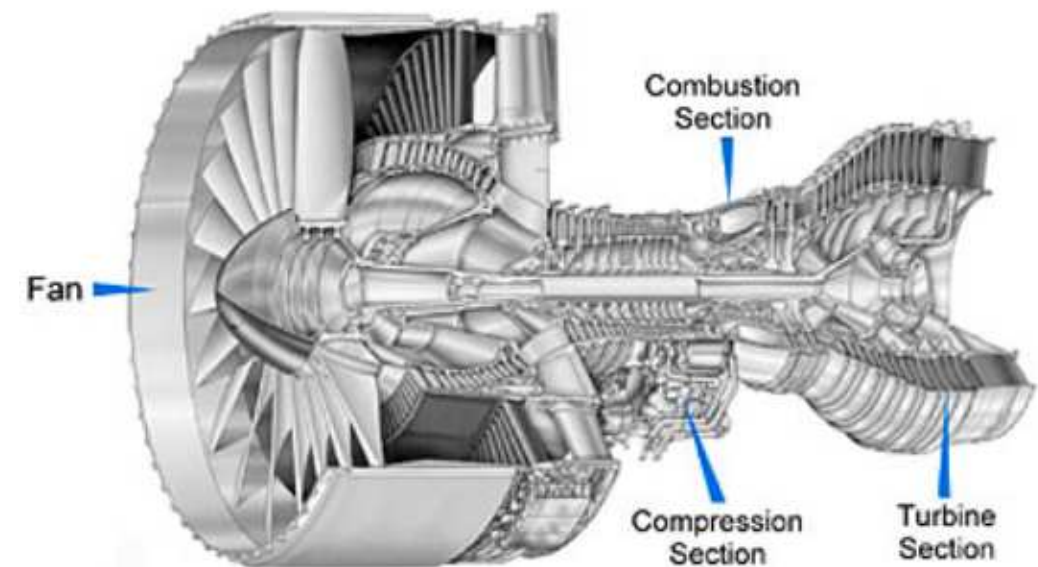
Introduction

- Numerical simulation can obtain the desired information and thus optimize the system

However, this approach requires well-defined boundary and operating conditions which may not be completely known due to limited access for experimental measurements



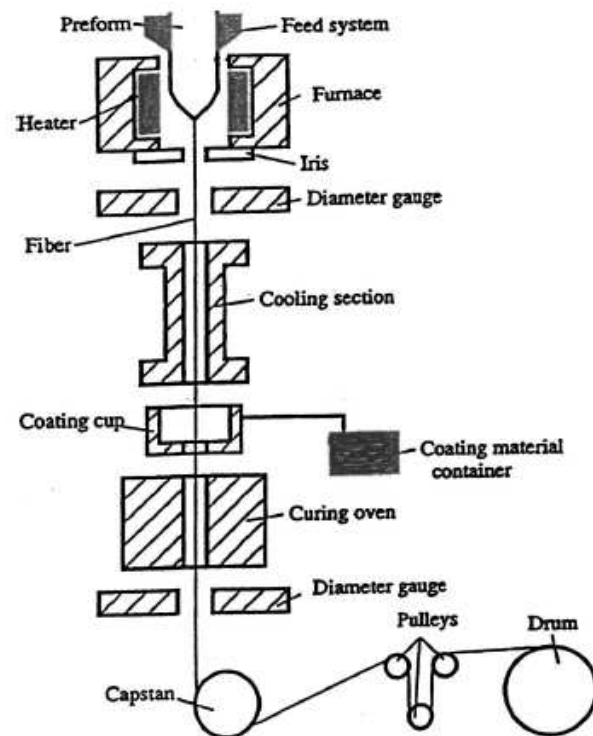
Optical fibre furnace



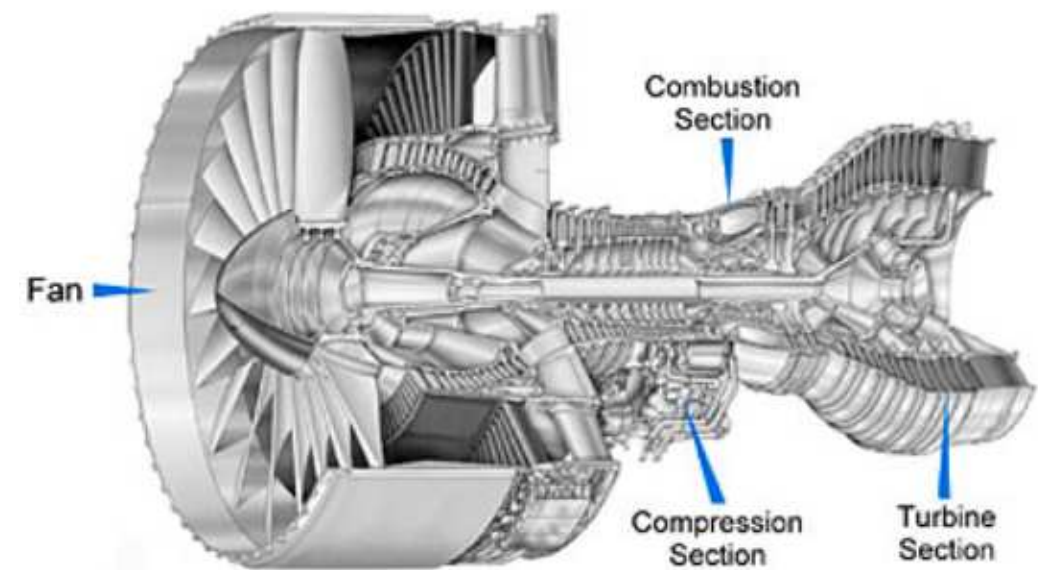
Turbofan engine

Introduction

- The objective of our research is to develop a Dynamic Data Driven Applications System approach that synergizes experiment and simulation to determine the boundary and operating conditions, thereby achieving a full simulation capability



Optical fibre furnace



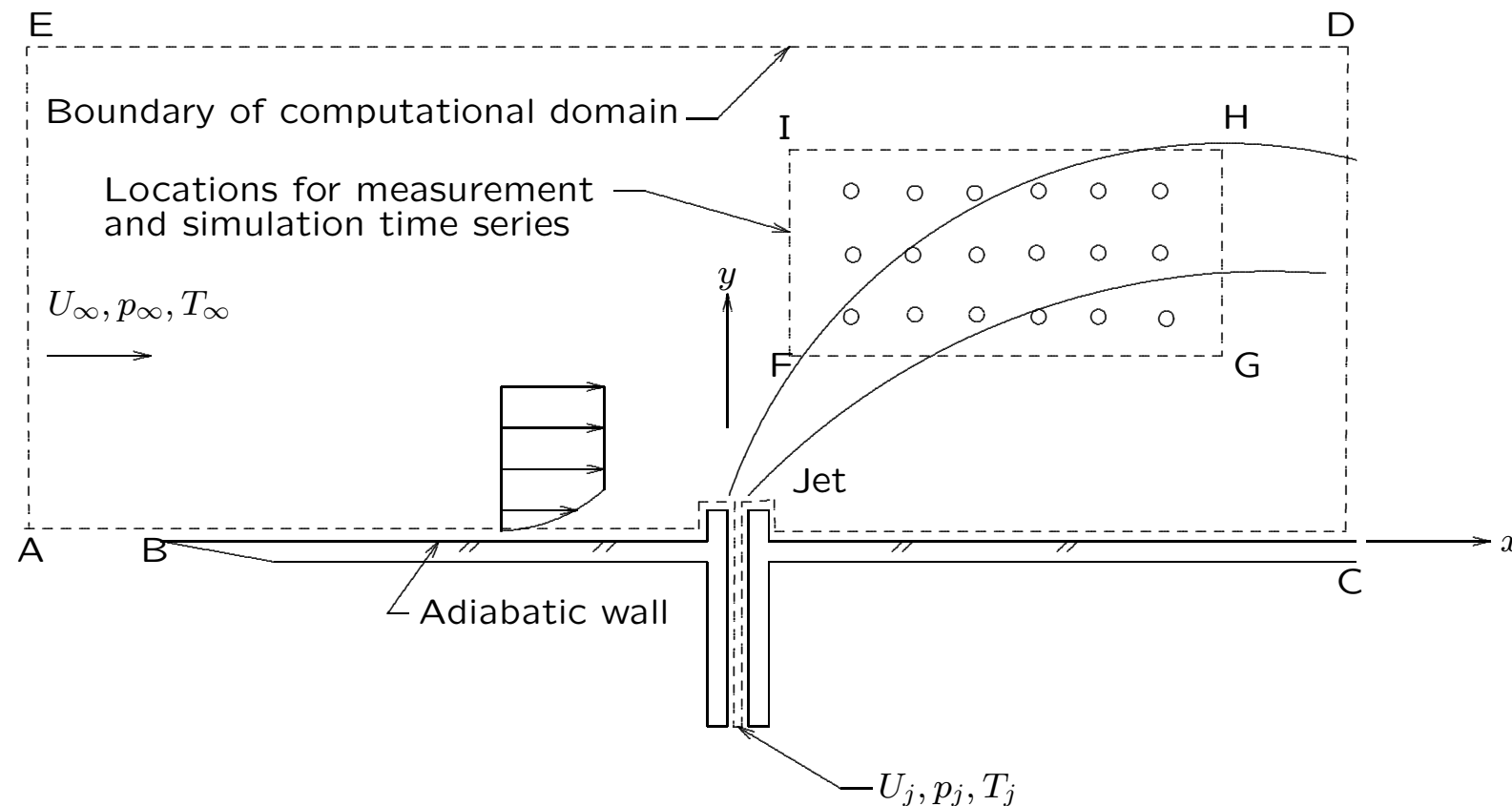
Turbofan engine

Problem Definition

Jet in Crossflow

- Heated wall jet in crossflow

The objective is to determine the jet inflow conditions (U_j , T_j) using a Dynamic Data Driven Applications Systems method that synergizes experiment and simulation



Item	Parameters	
	Known	Unknown
U_∞	✓	
T_∞	✓	
p_∞	✓	
U_j		✓
T_j		✓
p_j	✓	

Problem Definition

Jet in Crossflow

- Experiment

Rutgers Low Speed Wind Tunnel

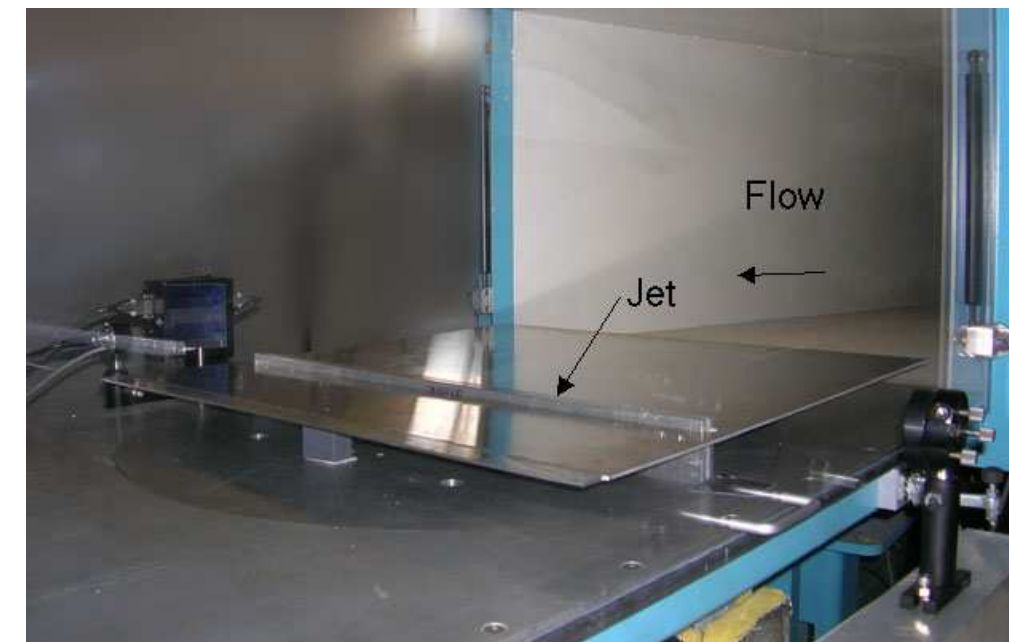
Non-intrusive laser diode measurement

Measure absorbance vs time at fixed (x, y)

Static temperature T vs time from absorbance

Limited region for absorbance measurement

Each (x, y) measurement requires ≈ 1 hr



Experimental configuration

Problem Definition

Jet in Crossflow

- Laser diode absorbance

Instantaneous absorbance

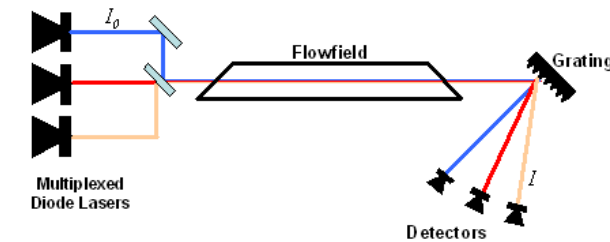
$$\mathcal{A}(x, y) = \frac{(I_o - I(x, y, t))}{I_o}$$

where I_o is incident intensity at (x, y, z_1) and $I(x, y, t)$ is transmitted intensity at (x, y, z_2)

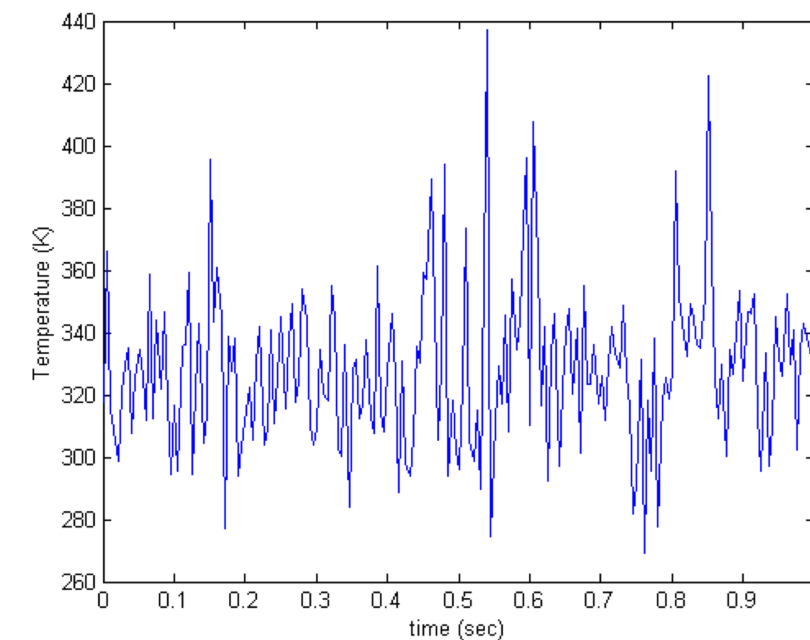
Absorbance per cm of the $^Q R_2(6)$ line of the oxygen transition $b_1 \Sigma_g^+ \nu' = 0 \leftarrow X^3 \Sigma_g^- \nu'' = 0$ at 761.139 nm is

$$\frac{d\mathcal{A}}{dz} = 0.083 T^{-1} - 2.26 \cdot 10^{-5}$$

where $T(x, y, z, t)$ is the static temperature in K



Laser diode arrangement

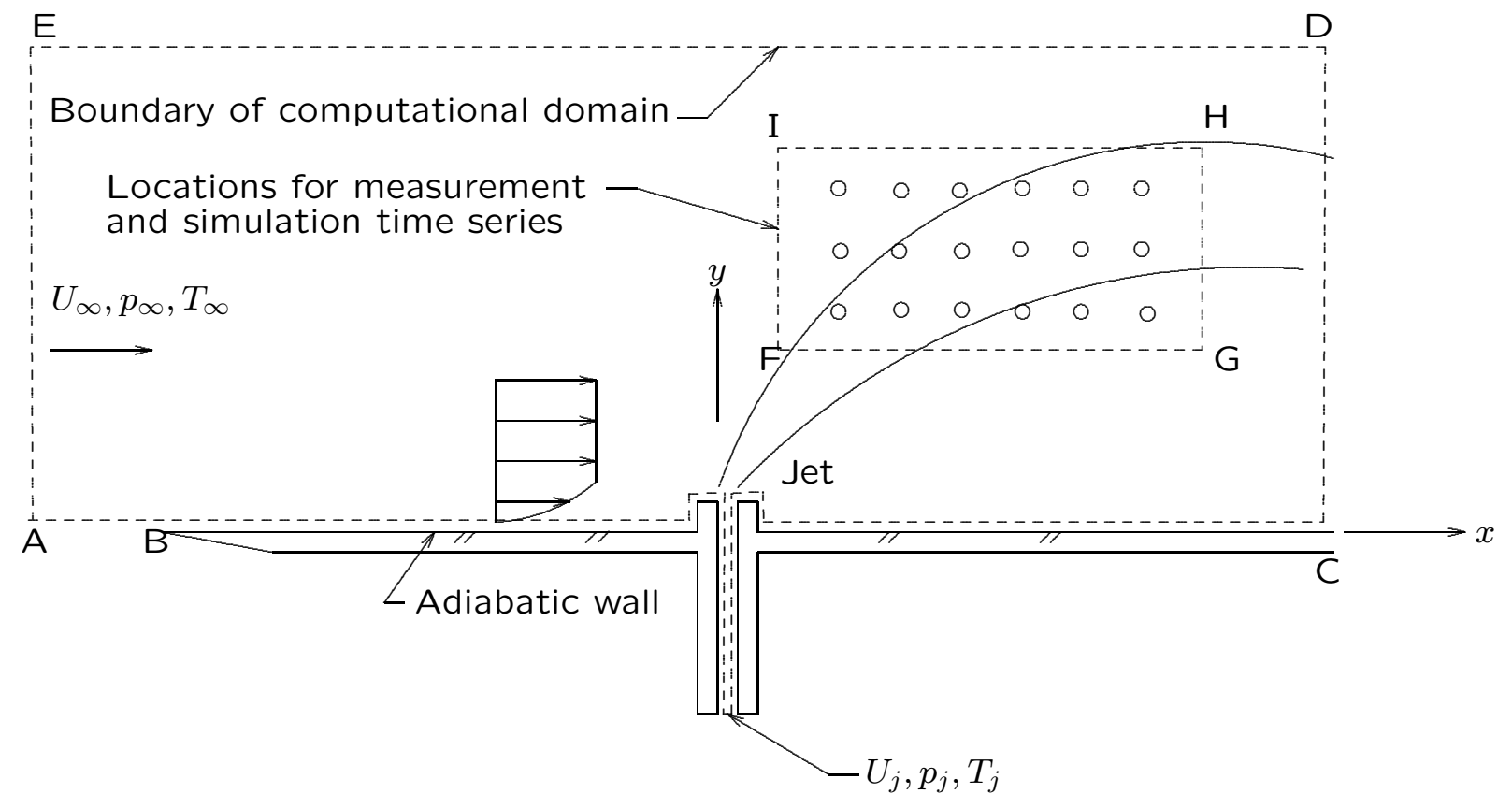


Typical T vs time

Problem Definition

Jet in Crossflow

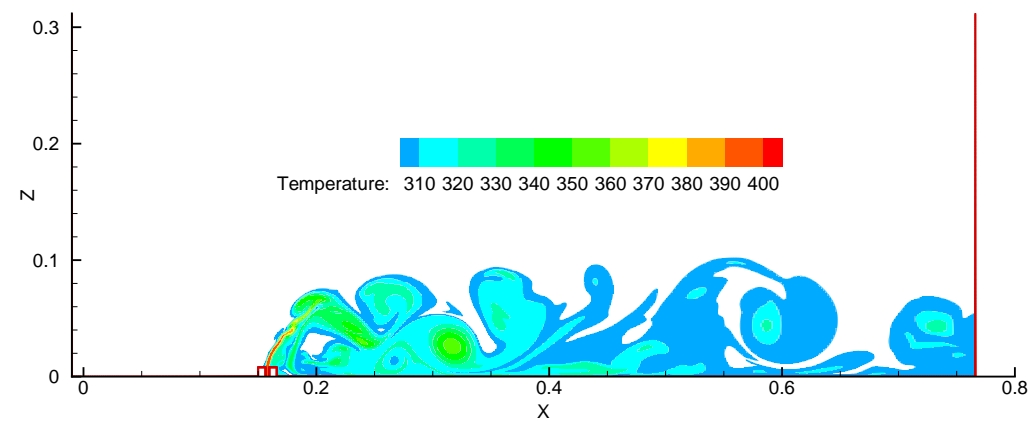
- Simulation
 - Laminar Navier-Stokes equations
 - Incompressible, ideal gas
 - Unsteady, time-dependent
 - Sutherland viscosity law
 - Fluent[©]
 - Parallel (8 processors)



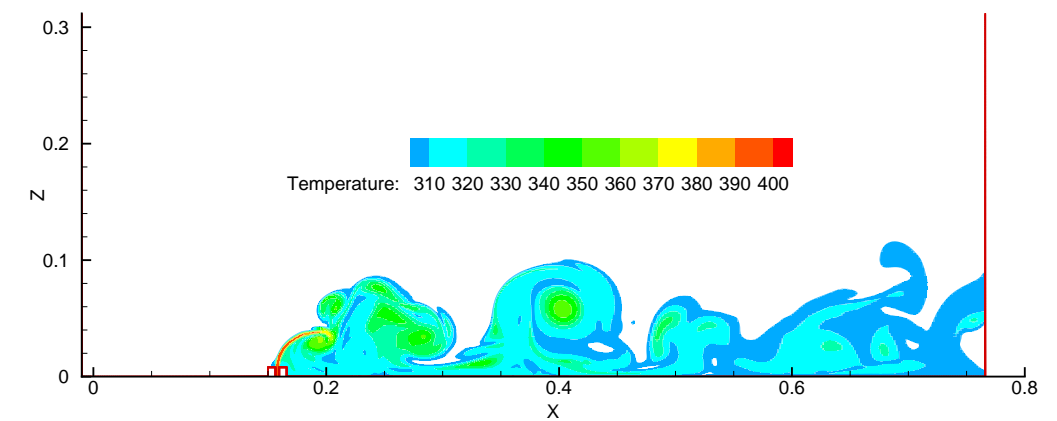
Problem Definition

Jet in Crossflow

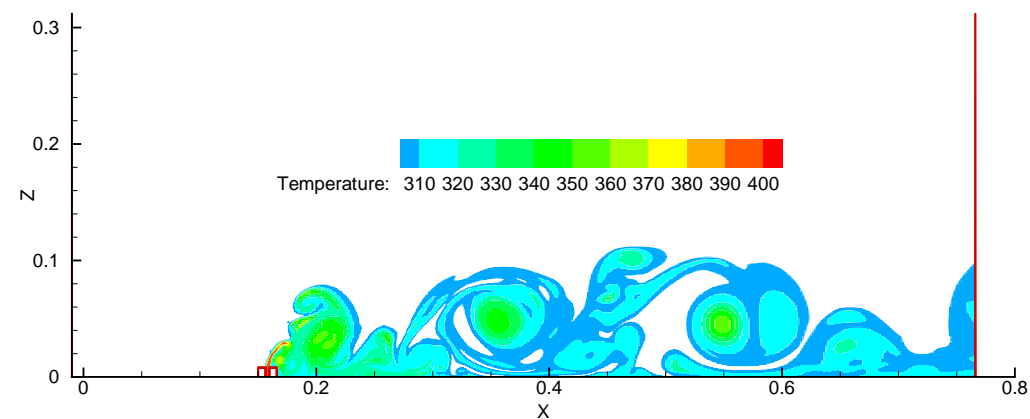
- Flow Structure



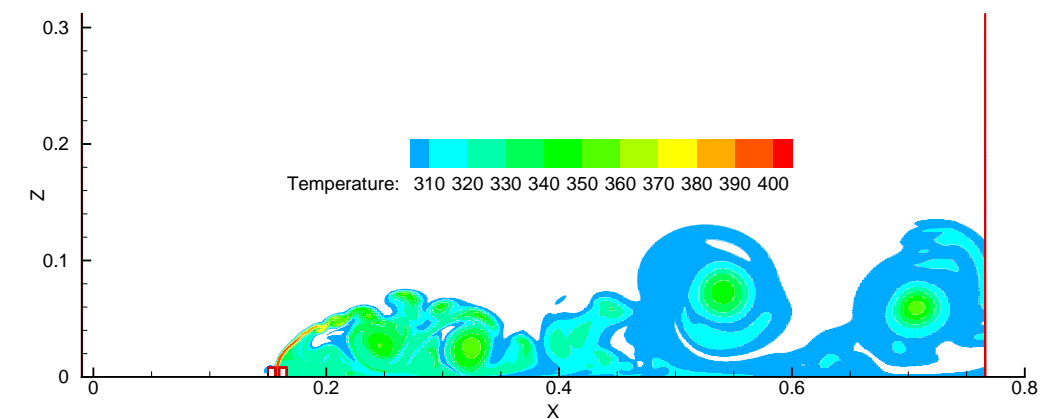
$t = 0$



$t = 40$ ms



$t = 80$ ms



$t = 120$ ms

Problem Definition

Jet in Crossflow

- Assumptions

Large set S_s of discrete data locations defined (\leq no. of grid cells in simulation)

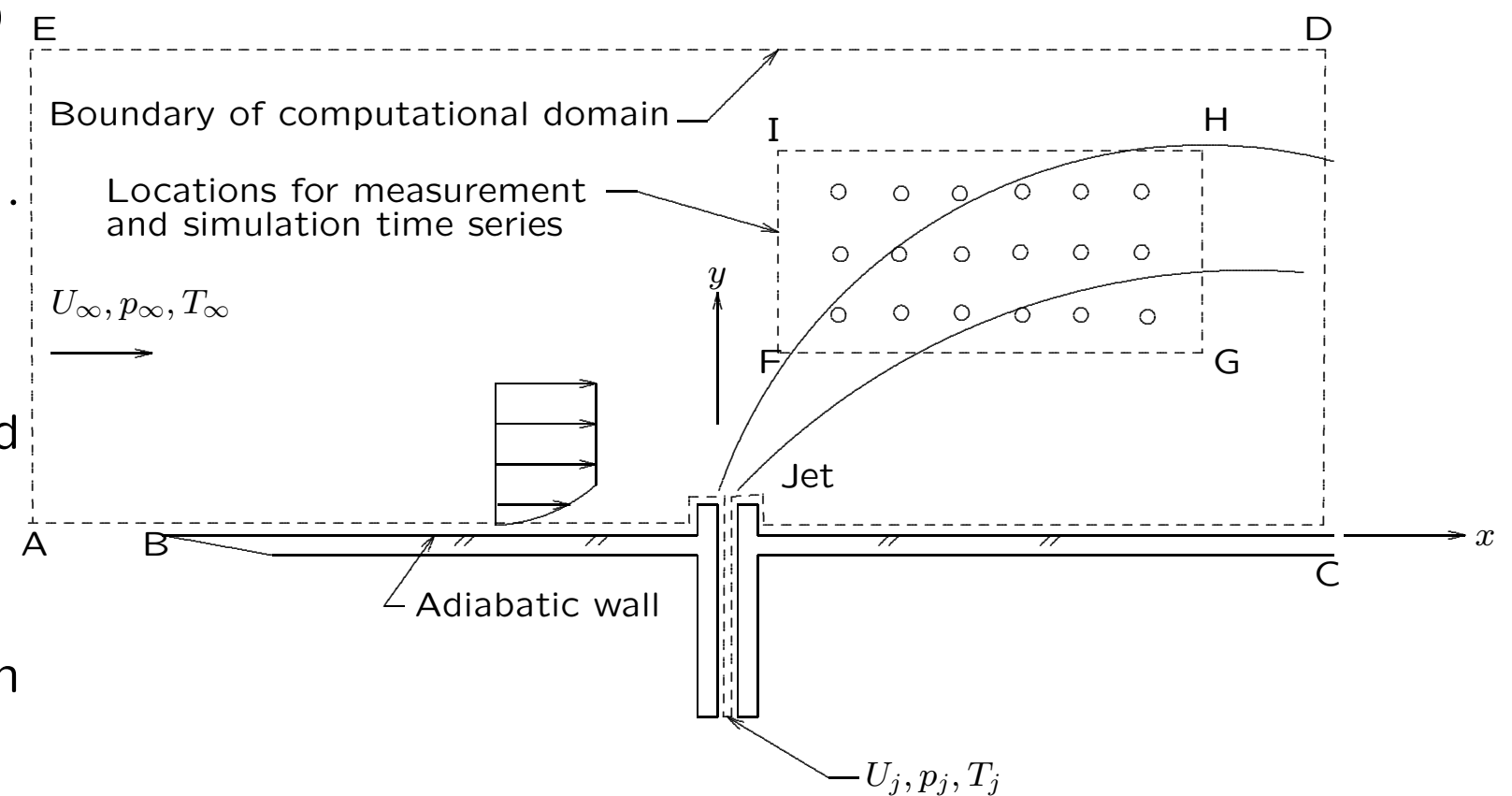
For each experiment, time series data obtained for small subset $S_e^k, k = 1, 2, \dots$ of locations

For each simulation, time series data obtained for entire set S_s for each U_j and T_j

- The quantity for comparison between experiment and simulation is the mean temperature $T_m(x, y)$

- Problem

Develop and apply a DDDAS Methodology for determining U_j and T_j



Response Surface Models

- Energy equation decouples from the mass and momentum equations
- Instantaneous temperature behaves as passive scalar and thus must scale as

$$T(x,y,t) - T_{\infty} = (T_j - T_{\infty})f(x,y,t; U_j, U_{\infty})$$

- Response Surface Model

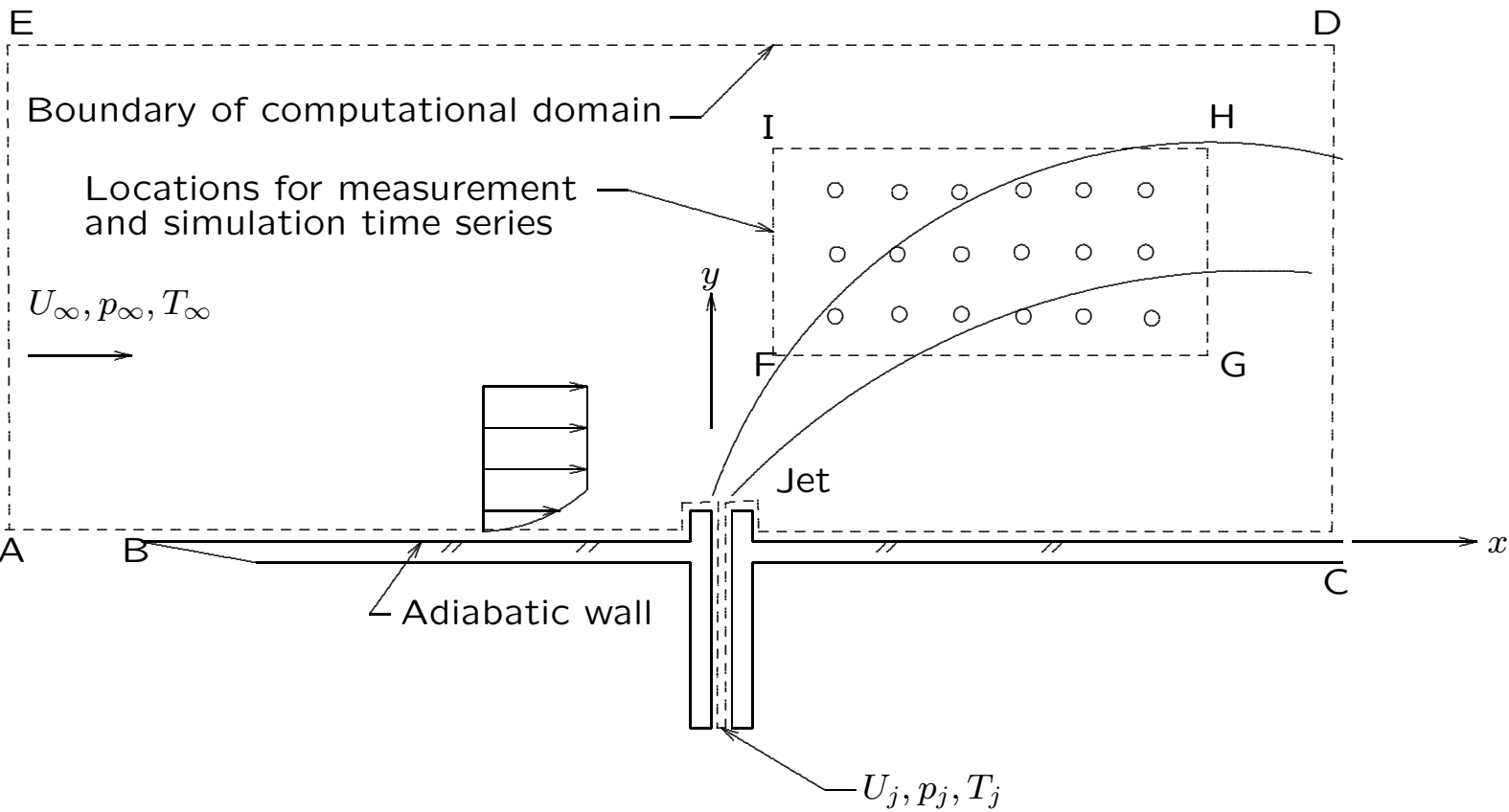
$$T_m(x,y)-T_{\infty} = \left(T_j - T_{\infty}\right) \left[\beta_o(x,y) + \beta_1(x,y) \left(\frac{U_j}{U_{\infty}}\right) + \beta_2(x,y) \left(\frac{U_j}{U_{\infty}}\right)^2\right]$$

- The coefficients $\beta_i(x,y)$ are obtained from simulations performed for a fixed value $T_j - T_{\infty}$ (selected from the range indicated in Table) and a set of U_j

Flow Conditions	
<i>Parameter</i>	<i>Value</i>
U_{∞} (m/s)	4.0
T_{∞} (K)	290.
p_{∞} (kPa)	101.8
U_j (m/s)	4.0 to 8.0
T_j (K)	350 to 450
p_j (kPa)	101.8

Dynamic Data Driven Applications System Methodology

1. Select monitor locations S_s for simulations
2. Generate Response Surface Models based on simulations for fixed ΔT_j^i
3. Select monitor locations S_e^k for experiments
4. Estimate experimental values for $T_j - T_\infty$ and U_j using Response Surface Models and experimental data at monitor locations
5. Repeat at Step No. 2 if estimated $T_j - T_\infty$ is significantly different than used to generate Response Surface Models; otherwise, determine new measurement locations S_e^{k+1}
6. Repeat until converged



No.	x	y	No.	x	y	No.	x	y
1	1.2	2.0	7	1.2	3.0	13	1.2	4.0
2	3.2	2.0	8	3.2	3.0	14	3.2	4.0
3	5.2	2.0	9	5.2	3.0	15	5.2	4.0
4	7.2	2.0	10	7.2	3.0	16	7.2	4.0
5	9.2	2.0	11	9.2	3.0	17	9.2	4.0
6	11.2	2.0	12	11.2	3.0	18	11.2	4.0

Distances in cm from jet center

Dynamic Data Driven Applications System Methodology

- Estimating experimental value of $T_j - T_\infty$ and U_j
 - Calculate square error between the experimental mean temperature and the Response Surface Model for each possible subset of l locations within S_e^k as computed as

$$E = \sum_l \left\{ \Delta T_{m_e} - \Delta T_j \left[\beta_0(x, y) + \beta_1(x, y) \left(\frac{U_j}{U_\infty} \right) + \beta_2(x, y) \left(\frac{U_j}{U_\infty} \right)^2 \right] \right\}^2$$

where $\Delta T_j = T_j - T_\infty$, $\Delta T_{m_e} = T_{m_e} - T_\infty$, and the sum is over l locations within S_e^k (the minimum number for l is 2)

Example: Assume S_e^k contains six locations and let $l = 2$. For each possible set of two locations from S_e^k , the values of ΔT_j and U_j that minimize E are determined. This yields fifteen triplets $(\Delta T_j, U_j, E)$.

- For a given value of l , the predicted values of ΔT_j and U_j , denoted by ΔT_j^l and U_j^l , are taken to be the triplet with the minimum E (i.e., the values of ΔT_j and U_j with the smallest square error).
- The procedure is repeated for all values of l from $l = 2$ to $n = \text{size } S_e^k$.
- The estimate for the experimental value of $T_j - T_\infty$ is the average of these values $T_j - T_\infty = (n-1)^{-1} \sum_{l=2}^n \Delta T_j^l$ and similarly for U_j .

Results

- Application of DDDAS Methodology

<i>No.</i>	<i>Step</i>	<i>Description</i>
1	1	A total of eighteen monitor locations were selected
2	2	Response Surface Models were generated at all monitor locations using $\Delta T_j = 66$ K
3	3	Six locations (Nos. 3, 9, 10, 14, 15 and 16) were selected for experiment
4	4	Using the experimental mean temperature measurements at the six locations, the estimated values $\Delta T_j = 110 \pm 16$ K and $U_j = 7.3 \pm 1$ m/s obtained using the RSMs
5	5	A new set of locations for experiments was defined based upon the RSMs (Nos. 2, 4, 5 and 17)
6	4	A revised estimate $\Delta T_j = 120 \pm 16$ K and $U_j = 7.1 \pm 1$ m/s obtained using the RSMs
7	2	A revised $T_j - T_\infty = 115$ K was selected for creation of the RSMs recognizing that the value originally used ($T_j - T_\infty = 66$ K) was far below the value predicted by the RSMs
8	4,5	The new RSMs yield the estimate $T_j - T_\infty = 105 \pm 13$ K and $U_j = 7.1 \pm 1$ m/s

- Result

<i>Quantity</i>	<i>Experiment</i>	<i>Predicted</i>
$T_j - T_\infty$	107 ± 10 K	105 ± 13 K
U_j	8.0 m/s	7.1 ± 1 m/s

Conclusions

- Developed DDDAS methodology for evaluation of fluid thermal systems
 - Examples are optical fibre furnace and turbofan combustor
 - Need for complete flowfield simulation to optimize system performance
 - Boundary conditions for flowfield simulation are not completely known *a priori*
 - Non-intrusive optical measurements (e.g., laser diode absorbance) feasible in limited region
 - DDDAS method to determine complete boundary conditions by synergizing experiment and simulation
- Developed DDDAS method to determining T_j and U_j
- DDDAS method predicts $T_j - T_\infty$ and U_j within experimental uncertainty